

(Following Paper ID and Roll No. to be filled in your
Answer Books)

Paper ID : 151854

Roll No.

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B.TECH.

Theory Examination (Semester-VIII) 2015-16

MULTIPHASE REACTOR DESIGN

Time : 3 Hours

Max. Marks : 100

Note: Attempt all three sections.

Section-A

1. Define the following: (2×10=20)

- (a) Catalyst Activity
- (b) Promoters and Inhibitors
- (c) Rate of Reaction
- (d) Comparision of Batch and Continuous flow reactors
- (e) Exothermic and Endothermic reactions

- (f) Yield and selectivity
- (g) Void fraction in catalyst pellet
- (h) Supported catalyst
- (i) Effect of temperature on Equilibrium conversion
- (j) Performance equation of Ideal Tubular Reactor

Section-B

2. Attempt any five parts of the following. (10×5=50)

- (a) Describe Multiphase reacting system. Mention two complicating factors that must be accounted for reactor design.
- (b) Write a short note on Optimum Temperature Progression and its importance for exothermic reactions in a reactor.
- (c) Describe the various methods of catalyst preparation.
- (d) List important characteristics of a catalyst and write the methods for their determination.
- (e) For a solid catalyzed reaction, discuss the heat effects during the reaction. Write equations for Particle ΔT and Film ΔT .

- (f) Describe the Shrinking Core Model for a fluid-particle non-catalytic reaction $A(g) + bB(s) \rightarrow \text{Products}$.
- (g) Describe an expression relating change in adiabatic temperature and equilibrium conversion.
- (h) Write the factors to be considered for selecting a contactor for gas-liquid reactions.

Section-C

Note: Attempt any two parts of the following. (15×2=30)

- 3. Show that $t/\tau = X_B$ for diffusion through gas film controlling the reaction rate, considering SCM for spherical particles of unchanging size in a fluid-particle non-catalytic reaction.
- 4. Discuss the reaction behavior from Instantaneous reactions to very slow reactions in a gas-liquid reaction and determine the location of the reaction zone.
- 5. Explain in detail, the method of Reactor design using Global rates of actual temperature and conversion profile.